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Attorney's Docket No.:	GK-BUE-103 / 500647.2	0004			
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International Application No.:	PCT/CH00/00317				
International Filing Date:	JUNE 09, 2000	09 JUNE 2000			
Priority Date Claimed:	AUGUST 18, 1999	18 AUGUST 1999			
Title of Invention:	PROCEDURE AND DEV PLASTIC MATERIAL	ICES FOR MANUFACTURING CRYST	ALLIZABLE		
Applicant(s) for (DO/EO/US):	Camille BORER; Mar	tin MUELLER and Frank GLOECH	NER		
Applicant herewith submits to	the United States Designated/Ele	cted Office (DO/EO/US) the following items and	other information:		
This is a SECOND or This express request examination until the A proper Demand for earliest claimed priori [Yes a copy of Publication a) _ is trans b) _ has bee c) _ is not re 371(c)(2)] A translation of Publication 371(c)(2)] Amendments to the cl a) _ are tran b) _ have bee c) _ have no d) _ have no d) _ have no d) _ have no A translation of the am [Yes a copy of Publication a) _ are trans b) _ have bee c) _ have no d) _ have no A translation of the am [Yes a copy of Publication a) _ are translation of the am A translation of the am (Amended sheets and	to begin national examination pro- expiration of the applicable time I International Preliminary Examin ty date. n No. WO 01/12698 published 2: mitted herewith (required only if r en transmitted by the international equired, as the application was file cation No. WO 01/12698 publish aims of the International Applicat nsmitted herewith (required only i en transmitted by the Internation t been made; however, the time I at been made and will not be made nendments to the claims under Po or declaration of the inventor(s) [3 nexes to the International Prelimi	ems concerning a filing under 35 U.S.C. 371. Decedures [35 U.S.C. 371 (f)] at any time rather the first set forth in 35 U.S.C. 371(b) and PCT Article attion was made by the 19th month from the action was made by the 19th month from the particular as filed [35] ot transmitted by the International Bureau and in the United States Receiving Office (RO/US) and 22FEB01 the International Application into Each of transmitted by the International Bureau and transmitted by the International Bureau and Bureau an	es 22 and U.S.C. 371(c)(2)]) English [35 U.S.C.		
An Information Disclost An Assignment docume included. [] 13 A FIRST preliminary A SECOND or SUB A substitute specificati A change of power of a [X] 16. (other items or informatical experiments of the content	v amendment SSEQUENT preliminary amendme on attorney and/or address letter	er sheet (PTO-1619A) in compliance with 37 CF. ent D: PCT/IB/308 22FEB01: PCT/IPFA			

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/Ruth Montalvo Date: February 13, 2002

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FAIER	APPROPRIATE BASIC FEE AMOUNT:			\$890.00	
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	Theck in the amount of \$1,170.00 to cover any additional fees required with this subm	aission or to credit any ove	erpayment to Deposit.	Account No: 50-15	29.)
NOTE: V	Where an appropriate time limit under 36 C (b)] must be filed and granted to restore the	FR 1.494 or 1.495 has not	been met a petition t	o revive [37 CFR 1.1	.37(a)
SEND AL Gerald h Reed Sm 375 Park	L CORRESPONDENCE TO: Kiel, Esq. (Customer No. 0)				
<u>Gerald H.</u> Name (Tel	Kiel (212) 521-5400) Signature	t-full		<u>bruary 13, 2002</u>	

EXPRESS MAILING CERTIFICATE

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D.C. 20231.

Ruth Montalvo

GK-BUE-103/500647.20004

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicants:

Camile BORER et al.

Group:

Unassigned

Serial No.:

10/049,549

Examiner:

Unassigned

Filing Date:

February 13, 2002

Customer No.: 026418

For:

PROCEDURE AND DEVICES FOR MANUFACTURING

CRYSTALLIZABLE PLASTIC MATERIAL

Commissioner for Patents Washington, D.C. 20231

PRELIMINARY AMENDMENT

Sir:

Prior to examination of the above-identified application on the merits, please amend the above-identified application as follows:

IN THE DRAWINGS:

Please delete the figure originally submitted in this application and substitute therefor the attached corrected Figure 1.

IN THE SPECIFICATION:

Please delete the specification and substitute therefor the attached substitute specification.

IN THE CLAIMS:

Before Claim 1, please delete "<u>CLAIMS</u>" and substitute therefor --<u>WHAT IS</u>

<u>CLAIMED IS:</u>--.

Please cancel Claims 1-8 and substitute therefor the following new Claims 9-27.

- --9. (New) A process for manufacturing crystallizable plastic material comprising:
 - (a) melting amorphous plastic material;
 - (b) pelletizing the plastic material;
 - (c) crystallizing the plastic material; and
 - (d) post-condensing the plastic material;

wherein the plastic material is not subjected to heating prior to the crystallization step and the plastic material is subjected to sieving after the crystallization step.--

- --10. (New) The process according to Claim 9, wherein the plastic material is a polyester.--
- --11. (New) The process according to Claim 10, wherein the polyester is polyethylene terephthalate.--

- --12. (New) The process according to Claim 9, wherein the crystallization step takes place at a temperature of 140 °C to 180 °C.--
- --13. (New) A device for manufacturing crystallizable plastic material for executing a process according to Claim 9, the device comprising a pelletizer, a fluidized bed (4) and a shaft reactor (7), wherein a sieve (5) is placed downstream from the fluidized bed (4).--
- --14. (New) The device according to Claim 13, wherein the plastic material is a polyester.--
- --15. (New) The device according to Claim 14, wherein the polyester is polyethylene terephthalate.--
- --16. (New) A process for manufacturing crystallizable plastic material comprising:
 - (a) melting amorphous plastic material;
 - (b) crystallizing the plastic material;
 - (c) pelletizing the plastic material; and
 - (d) post-condensing the plastic material:

wherein the plastic material is not warmed again prior to the crystallization step and the plastic material is subjected to sieving after the pelletization step at roughly the same temperature as during the crystallization step and the pelletization step.--

- --17. (New) The process according to Claim 16, wherein the temperature during the crystallization step, the pelletization step and the sieving step is between $100~^{\circ}\text{C}$ and $200~^{\circ}\text{C}$.
- --18. (New) The process according to Claim 16, wherein the temperature during the crystallization step, the pelletization step and the sieving step is between 120 $^{\circ}$ C and 160 $^{\circ}$ C.--
- --19. (New) The process according to Claim 16, wherein retention time during the crystallization step is approximately 1 to 40 seconds. --
- --20. (New) The process according to Claim 16, wherein retention time during the crystallization step is approximately 2 to 20 seconds.--
- --21. (New) The process according to Claim 16, wherein the sieving step is followed by a second crystallization step.--
- --22. (New) The process according to Claim 16, wherein the plastic material is a polyester.--
- --23. (New) The process according to Claim 22, wherein the polyester is polyethylene terephthalate.--
- --24. (New) A device for manufacturing crystallizable plastic material, for executing a process according to Claim 16, comprising a first crystallizer and a downstream cutter (2), wherein a sieve (5) is placed downstream from the cutter (2).--

- --25. (New) The device according to Claim 24, wherein a second crystallizer is placed downstream from the sieve (5).--
- --26. (New) The device according to Claim 24, wherein the plastic material is a polyester.--
- --27. (New) The device according to Claim 26, wherein the polyester is polyethylene terephthalate.--

REMARKS

As a result of the foregoing amendment, Claims 1-8 have been cancelled and Claims 9-27 have been added. Accordingly, Claims 9-27 are pending in this application.

Applicants have hereinabove amended the drawings to delete the originally filed figure and substitute therefor a corrected figure (Figure 1). No new matter has been added in Figure 1.

Applicants have also hereinabove amended the specification to more particularly describe the prior art, to add section headings, to add a brief description of the figure and to correct spelling and/or grammatical errors. Further, as several amendments have been made to the specification, Applicants have submitted herewith a substitute specification. Applicants have also attached herewith a copy of the specification as it existed prior to this Preliminary Amendment with the changes made in the substitute specification

shown with brackets and underlines. No new matter has been added in the substitute

specification.

As stated above, Applicants have hereinabove amended the claims to delete

Claims 1-8 and substitute therefor new Claims 9-27. In particular, Applicants have

substituted the new claims for the original claims to provide antecedent basis for several

terms and to conform the claims to U.S. patent practice. Applicants have enclosed a fee

supported by the original specification and claims. No new matter has been added in the new

claims.

In view of the foregoing, it is submitted that this application is now in

condition for examination on the merits and prompt notice of allowance is earnestly solicited.

Respectfully submitted,

REED SMITH, LLP

March 21, 2002

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GHK/SRP:dw

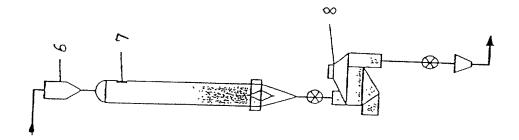
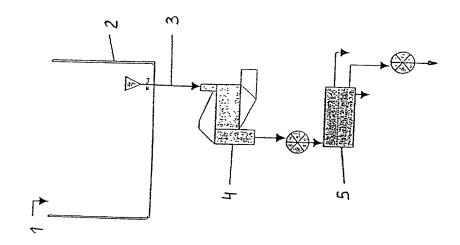


FIGURE 1



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WO 01/12698 PCT/CH00/00317

Procedure and Device for Manufacturing Crystallizable Plastic Material

The invention relates to a procedure for manufacturing crystallizable plastic material, such as polyesters and the like, in particular PET, by having the melting phase be followed by crystallization and solid-state post-condensation phase, as well as to a device for executing the procedure.

Crystallization and solid-state post-condensation (SSP) of polyesters obtained from a melt, in particular PET (polyethylene terephthalate), is generally known). In this case, the meltable polyester (melting point 270 °C and above) is processed into cylindrical pellets while simultaneously cooled down to room temperature, and serves as an amorphous parent material for subsequent crystallization and post-condensation to PET. According to EP-A-379684, crystallization takes place in two fluidized beds (combination of solids-air bed and boiling bed) at temperatures of 140 °C to 180 °C. Crystallization is followed by exposure to impact to dissolve agglomerates.

However, crystallizing at a temperature of less than $140\,^{\circ}\text{C}$ already and also executing solid-state post-condensation at a temperature exceeding $180\,^{\circ}\text{C}$ is also known (e.g., according to CH 02131/92-2, which was not published as prior art).

EP-A-822214 describes a procedure in which polyester material is extruded, pelleted and crystallized without cooling the melt to a temperature far below the crystallization point. In this case, a temperature of

... a conventional SSP process for 24 hours at approx. 205 °C. According to the instruction of US-A-5510454, the temperature of the plate onto which the drops fall can also measure 180 °C.

Also known is a procedure for the simultaneous drying and crystallization of thermoplastics, e.g., PET according to WO94/25239, wherein plastic filaments to be dried are quenched for at most 1.5 seconds to achieve a surface temperature of at least 100 °C. As a result of this only partial cooling of the plastic, the crystallization period is to measure at most 20 seconds.

In a device for manufacturing polyamides according to DE-A-19510698, a moving-bed reactor can be evacuated, wherein an evacuation pump can be provided with a separator for separating dust out of the waste gas. However, solid foreign substances, dusts and the like are not reliably removed from the plastic material.

US-3405098 describes a procedure for preparing linear condensation polyesters for solid phase polymerization, wherein the melt is quickly quenched in order to obtain an essentially amorphous, solid polyester, which is subsequently heated to 150 °C to 200 °C again, in order to obtain a partially crystallized polyester, which is subsequently milled into fine particles, and classified using sieves. The polyester prepared in this away is then subjected to solid-phase polymerization in a fluidized bed.

The object of the invention is to further develop a procedure for manufacturing crystallizable plastic material, like polyester or PET, in such a way as to achieve a higher reactivity in the SSP process as the result of larger crystals and an improved surface

crystal structure, and to reliably separate solid foreign substances form the plastic material after crystallization. Power consumption is to be reduced as well. This is done based on the features in claims 1 or 3.

The object of the invention is also to provide a suitable device for executing the above procedure.

The subclaims contain preferred embodiments.

The invention shall be described in greater detail below in an embodiment based on a drawing. The sole figure in the drawing shows an elementary diagram.

PET 1 passes from a melting reactor (not shown) into a cutter 2 with a temperature of approx. 280 °C while being cooled and solidified.

The amorphous pellets 3 with a temperature of 140 °C to 180 °C produced in this way then pass to a fluidized bed 4 without any further cooling for a retention time typical for the procedure, and then to a sieve 5, which can also have a downstream ambient air sifter to separate out dust and other foreign solids.

According to EP-A-379684, the fluidized bed 2 can also resemble a combination of spouted bed and boiling bed. If needed, additional crystallization can follow the sieving process (not shown).

The PET cleaned and crystallized in this way passes in the usual manner into a preheater 6, or directly into a shaft reactor 7, where the solid phase recondensation into PET takes place, and only thereafter is the granulate cooled to room temperature in a cooler 8.

CLAIMS

- 1. A procedure for manufacturing crystallizable plastic material, such as polyesters, e.g., PET, by melting on amorphous plastic material, which is subsequently granulated, crystallized and recondensed, wherein the plastic material need not be heated before crystallization, characterized in that the plastic material is subjected to a sieving process after crystallization, and that crystallization takes place at a temperature of 140 °C to 180 °C.
- 2. A device for manufacturing crystallizable plastic material, such as polyester, e.g., PET, for executing a procedure according to claim 1, comprising a granulating device, a fluidized bed (4) and a shaft reactor (7), characterized in that a sieve (5) is placed downstream from the fluidized bed (4).
- 3. procedure for manufacturing crystallizable plastic material, such as polyester, e.g., PET, by melting amorphous plastic material, which subsequently crystallized, granulated recondensed, wherein the plastic material need not be heated again before crystallization, characterized by the fact that, after granulation, the plastic material is subjected to a sieving process at about the same temperature as during crystallization and granulation.
- 4. The procedure according to claim 3, characterized in that the temperature during crystallization, granulation and sieving measures 100 °C to 200 °C, preferably 120 °C to 160 °C.

- 5. The procedure according to one of claims 3 or 4, characterized in that the retention time during crystallization measures approx. 1 to 40 seconds, preferably 2 to 20 seconds.
- 6. The procedure according to claim 5, characterized in that the sieving process is followed by further crystallization.
- 7. A device for manufacturing crystallizable plastic material, such as polyester, e.g., PET, for executing a procedure according to claim 3, with a crystallizer followed by a cutter (2), characterized in that a sieve (5) is placed downstream from the cutter (2).
- 8. The device according to claim 7, characterized in that another crystallizer is placed downstream from the sieve (5).





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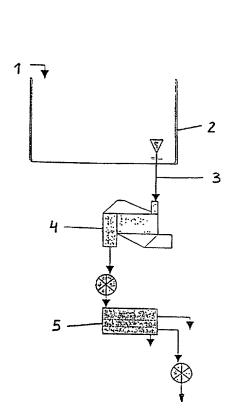
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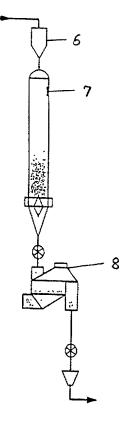
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[Fortsetzung auf der nächsten Seite]

(54) Title: METHOD AND DEVICE FOR PRODUCING CRYSTALLISABLE PLASTIC MATERIAL

(54) Bezeichnung: VERFAHREN UND VORRICHTUNG ZUR HERSTELLUNG VON KRISTALLISATIONSFÄHIGEM KUNSTSTOFFMATERIAL

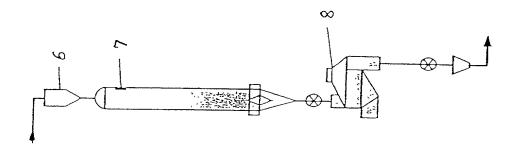


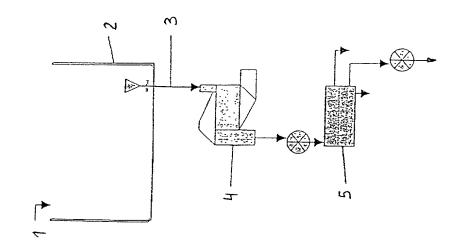


(57) Abstract: The invention relates to a method and a device for producing crystallisable plastic material, especially PET, by means of a conventional SSP treatment. The plastic material only cools down to the crystallisation. After granulation and crystallisation, the plastic material is subjected to a sieving process in a temperature remaining approximately the same.

(57) Zusammenfassung: Die Erfindung betrifft ein Verfahren und eine Vorrichtung zur Herstellung von kristallisationsfähigem Kunststoffmaterial, insbesondere von PET mittels einer üblichen SSP-Behandlung, wobei das Kunststoffmaterial vor der Kristallisation nur bis auf Kristallisationstemperatur abkühlt und nach dem Granulieren und Kristallisieren bei etwa gleichbleibender Temperatur einem Siebvorgang unterzogen wird.

1/1





10/049549

Sub Spec

PROCEDURE AND DEVICE FOR MANUFACTURING CRYSTALLIZABLE PLASTIC MATERIAL

BACKGROUND OF THE INVENTION

The present invention relates to a procedure for manufacturing crystallizable plastic material, e.g., polyesters and the like, and in particular polyethylene terephthalate (PET), via post-melting phase crystallization and solid-phase post-condensation, and a device for executing the procedure.

The crystallization and post-condensation in the solid-phase (SSP) of polyesters obtained from a melt, in particular PET (polyethylene terephthalate), is generally known. In this case, the melted polyester (melting point 270 °C and [above] higher) is processed into cylindrical pellets, for example, while simultaneously cooled down to room temperature, and serves as an amorphous starting material for subsequent crystallization and post-condensation to PET. According to EP-A-379684, for example, crystallization takes place in two fluidized beds (combination of boiling and spouting beds) at temperatures of 140 °C to 180 °C. Crystallization is followed by exposure to impact to dissolve agglomerates.

However, it is also known that crystallization can take place at a temperature of less than 140 °C and solid-state post-condensation can take place at a temperature exceeding 180 °C (e.g., according to the unpublished CH 02131/92-2).

EP-A-822214 describes a procedure in which a polymer is extruded, pelleted and crystallized without material far below cooling the melt to a temperature crystallization temperature. In this case, a temperature of approx. 160 °C to 220 °C is maintained, and crystallization takes approx. 5 - 30 minutes. However, WO 97/23543 discloses omission of strong cooling off during pelleting. this Polyester is kept in a melt at approx. 270 °C, and drips through a hole onto a hot (approx. 135 °C) metal plate, where crystallization has already taken place. A conventional SSP process then follows this for 24 hours at approx. 205 °C. According to U.S. Patent No. 5,510,454, the temperature of the plate that receives the drops can also measure 180 °C.

Also known is a procedure for the simultaneous drying and crystallization of thermoplastics, e.g., PET according to WO94/25239, wherein plastic strands to be dried are quenched for at most 1.5 seconds to achieve a surface temperature of at least 100 °C. This partial cooling of the

plastic only reduces the crystallization time down to approx.

20 seconds at most.

In a device for manufacturing polyamides according to DE-A-19510698, a moving-bed reactor can be evacuated, wherein a vacuum pump can be provided with a separator for separating dust from the waste gas. However, solid foreign substances, dusts and the like are not reliably removed from the plastic material.

Further, U.S. Patent No. 3,405,098 describes a procedure for preparing linear condensation polyesters for solid phase polymerization, wherein the melt is quickly quenched in order to obtain an essentially amorphous, solid polyester, which is subsequently heated to 150 °C to 200 °C again, in order to obtain a partially crystallized polyester, which is subsequently milled into fine particles, and classified using sieves. The polyester prepared in this way is then subjected to solid-phase polymerization in a fluidized bed.

SUMMARY OF THE INVENTION

One of the objects of the present invention is to further develop a procedure for manufacturing crystallizable plastic material, such as polyester or PET, in such a way as

to achieve a higher reactivity in the SSP process through larger crystallites and improved surface crystal structure, and to reliably separate solid foreign substances from the plastic material after crystallization.

Another object of the present invention is to lower power consumption. This is accomplished based upon the features described in the claims.

Another object of the present invention is to provide a suitable device for executing the above procedure.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 shows a schematic view of an embodiment of the present invention.

DETAILED DESCRIPTION OF THE INVENTION

Preferred embodiments of the present invention are described in the claims.

The present invention shall be described in greater detail based upon the embodiment shown in Figure 1. Figure 1 shows a schematic view of the embodiment.

In particular, PET 1 exits a melt reactor (not shown) and enters a cutter 2 at a temperature of approx. 280 °C while being cooled and solidified.

The amorphous pellets 3 having a temperature of 140 °C to 180 °C generated in this way then pass to a fluidized bed 4 without further cooling, and subsequently to a sieve 5, which can be followed by a recirculating air sifter if required, in order to separate out dust and other foreign solids.

According to EP-A-379684, the fluidized bed 2 can also be a combination of boiling and spouted beds. If need be, the sieving process is followed by more crystallization (not shown).

The PET cleaned and crystallized passes in a conventional manner to a preheater 6 or directly to a shaft reactor 7, where the solid phase post-condensation into PET takes place, and only thereafter are the pellets cooled to room temperature in a cooler 8.

MATERIAL

BACKGROUND OF THE INVENTION

The present invention relates to a procedure for manufacturing crystallizable plastic material, [such as] e.g., polyesters and the like, and in particular [PET] polyethylene terephthalate (PET), [by having the melting] via post-melting phase [be followed by] crystallization and [solid-state] solid-phase post-condensation [phase, as well as to], and a device for executing the procedure.

[Crystallization] The crystallization and [solid-state] postcondensation in the solid-phase (SSP) of polyesters obtained from a melt, in particular PET (polyethylene terephthalate), is generally known[)]. In this case, the [meltable] melted polyester (melting point 270 °C and [above] higher) into cylindrical pellets, for example, processed simultaneously cooled down to room temperature, and serves as [parent] starting material for subsequent amorphous crystallization and post-condensation to PET. According to EP-A-379684, for example, crystallization takes place in two fluidized beds (combination of [solids-air bed and] boiling [bed] and spouting beds) at temperatures of 140 °C to 180 °C. Crystallization is followed by exposure to impact to dissolve agglomerates.

However, [crystallizing] it is also known that crystallization can take place at a temperature of less than 140 °C [already] and [also executing] solid-state post-condensation can take place at a temperature exceeding 180 °C [is also known] (e.g.,

according to the unpublished CH 02131/92-2[, which was not published as prior art]).

EP-A-822214 describes a procedure in which [polyester] a material is extruded, pelleted and crystallized without cooling the melt to a temperature far below the In this case, temperature. crystallization [point] temperature of approx. 160 °C to 220 °C is maintained, and crystallization [is to take] takes approx. 5 - 30 minutes. 97/23543 [already disclosed] <u>discloses</u> However, WO [process] omission of strong cooling off during pelleting. Polyester is [held] kept in a melt at approx. 270 °C, and drips through [an opening] a hole onto a [metal plate heated to] hot (approx. 135 °C) metal plate, where crystallization has already taken place. [This is then followed by al [takes] conventional SSP process then follows this for 24 hours at approx. 205 °C. According to [the instruction of US-A-5510454] U.S. Patent No. 5,510,454, the temperature of the plate [onto which the drops fall] that receives the drops can also measure 180 °C.

Also known is a procedure for the simultaneous drying and crystallization of thermoplastics, e.g., PET according to WO94/25239, wherein plastic [filaments] strands to be dried are quenched for at most 1.5 seconds to achieve a surface temperature of at least 100 °C. [As a result of this only] This partial cooling of the plastic[,] only reduces the crystallization [period is to measure at most] time down to approx. 20 seconds at most.

In a device for manufacturing polyamides according to DE-A-19510698, a moving-bed reactor can be evacuated, wherein [an evacuation] a vacuum pump can be provided with a separator for separating dust [out of] from the waste gas. However, solid

foreign substances, dusts and the like are not reliably removed from the plastic material.

[US-3405098] Further, U.S. Patent No. 3,405,098 describes a procedure for preparing linear condensation polyesters for solid phase polymerization, wherein the melt is quickly quenched in order to obtain an essentially amorphous, solid polyester, which is subsequently heated to 150 °C to 200 °C again, in order to obtain a partially crystallized polyester, which is subsequently milled into fine particles, and classified using sieves. The polyester prepared in this [away] way is then subjected to solid-phase polymerization in a fluidized bed.

SUMMARY OF THE INVENTION

[The object] One of the objects of the present invention is to further develop a procedure for manufacturing crystallizable plastic material, [like] such as polyester or PET, in such a way as to achieve a higher reactivity in the SSP process [as the result of] through larger [crystals] crystallites and [an] improved surface crystal structure, and to reliably separate solid foreign substances [form] from the plastic material after crystallization. [Power consumption is to be reduced as well. This is done based on the features in claims 1 or 3.]

Another object of the present invention is to lower power consumption. This is accomplished based upon the features described in the claims.

[The] <u>Another</u> object of the <u>present</u> invention is [also] to provide a suitable device for executing the above procedure.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 shows a schematic view of an embodiment of the present invention.

DETAILED DESCRIPTION OF THE INVENTION

[The subclaims contain preferred] <u>Preferred</u> embodiments of the <u>present invention are described in the claims</u>.

The <u>present</u> invention shall be described in greater detail [below in an embodiment based on a drawing] <u>based upon the embodiment shown in Figure 1</u>. [The sole figure in the drawing shows an elementary diagram.] <u>Figure 1 shows a schematic view of the embodiment.</u>

In particular, PET 1 [passes from] exits a [melting] melt reactor (not shown) [into] and enters a cutter 2 [with] at a temperature of approx. 280 °C while being cooled and solidified.

The amorphous pellets 3 [with] having a temperature of 140 °C to 180 °C [produced] generated in this way then pass to a fluidized bed 4 without [any] further cooling [for a retention time typical for the procedure], and [then] subsequently to a sieve 5, which can [also have a downstream ambient] be followed by a recirculating air sifter if required, in order to separate out dust and other foreign solids.

According to EP-A-379684, the fluidized bed 2 can also [resemble] be a combination of [spouted bed and boiling bed] boiling and spouted beds. If [needed] need be, [additional]

crystallization can follow] the sieving process <u>is followed by</u> more crystallization (not shown).

The PET cleaned and crystallized <u>passes</u> in [this way passes in the usual] <u>a conventional</u> manner [into] <u>to</u> a preheater 6[,] or directly [into] <u>to</u> a shaft reactor 7, where the solid phase [recondensation] <u>post-condensation</u> into PET takes place, and only thereafter [is the granulate] <u>are the pellets</u> cooled to room temperature in a cooler 8.

UNITED STATES OF AMERICA COMBINED DECLARATION AND POWER OF ATTORNEY FOR PATENT APPLICATION

FILE NO. GK-BUE-103/ 500647.20004

As a below named inventor, I hereby declare that: my residence, post office address and citizenship are as stated below next to my name; that I verily believe that I am the original, first and sole inventor (if only one name is listed below) or a joint inventor (if plural inventors are named) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

PROCEDURE AND DEVICE FOR MANUFACTURING CRYSTALLIZABLE PLASTIC MATERIAL				
The specification of which				
and was amended on _	as United States pa 2000 as PCT international pat (i	ii aiiy).		
I hereby state that I have reviewe claims, as amended by any amer	ament referred to above.			
I acknowledge the duty to disclos of Federal Regulations, § 1.56.				
I hereby claim foreign priority ber of inventor's certificate listed belocertificate having a filing date before	w and have also identified held	iw anv ioreion abblica	ILIOH IOI Daici	olication(s) for patent nt or inventor's
Prior Foreign Application(s)	A TO A TION AND HADED	DATE OF FILING	-	PRIORITY
COUNTRY	APPLICATION NUMBER	(day, month, year)		CLAIMED UNDER 35 U.S.C. § 119
Germany	199 38 583.1	18 August 19	99	YES _x NO
14.	,			YES NO
hereby appoint REED SMITH LLP a 24,408; Gerald H. Kiel, Reg. No. 25, Reg. No. 24,403; Daniel Lent, Reg attorneys with full power of substitut therewith and to receive all correspondents.	,116; Eugene LeDonne, Reg. No. . No. <u>44,867;</u> Samir R. Patel, Region and revocation to prosecute alondence.	35,930, Stephen Chin,	ny K Ahn Re	g No 40 243 as
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DII	RECT TELEPHONE CALLS TO: (2	212) 521-5400		
I hereby declare that all statemer belief are believed to be true; and fu like so made are punishable by fine such willful false statements may je	or imprisonment or both linder S	Rection 1001 of Title 18	of the United	
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F ATTORNEY	File No. (2K_BHE_103/	
COMBINED DECLARATION AND POWER OF ATTORNEY FOR PATENT APPLICATION (continued)		File No. GK-BUE-103/ 500647.20004	
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